



bioenergy2020+

# Biogas from organic residues and outlook on heterofermentative alcohol production

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IEA RESEARCH  
COOPERATION

# Why anaerobic fermentation



- Degradation of organic substances
  - Reduction of waste
- Reduction of green house gases
- Energy production
  - Gaseous
  - Liquid
- Production of fertiliser



# AD plants in Austria



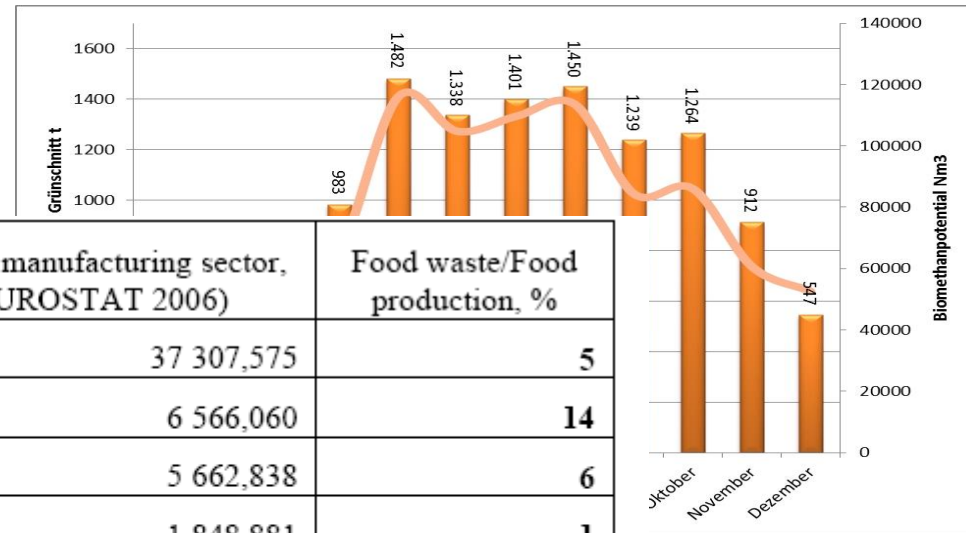
Substrate / Plant type	Number of plants	Mio. Nm <sup>3</sup> biogas per year	% Percentage
Landfill	62	45 - 100	21
Sewage sludge	134	75 - 100	26
Agricultural plants (including co-digestion)	350	121 - 182	45
Industry (including anaerobic wastewater pre-treatment)	25	9 - 14	3
Plants from municipalities and waste associations	15	15 - 18	5
<b>TOTAL</b>	<b>586</b>	<b>265 - 414</b>	<b>100</b>

# Potentials organic residues



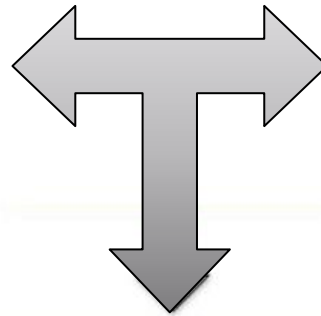
- Organic waste from households
  - Methane yield 70-80 Nm<sup>3</sup>/t FM

- Organic residues from industry



	Food production, tonnes (EUROSTAT 2006)	Food waste in manufacturing sector, tonnes (EUROSTAT 2006)	Food waste/Food production, %
<b>EU27</b>	766 179,686	37 307,575	<b>5</b>
Poland	47 233,940	6 566,060	<b>14</b>
Italy	97 088,841	5 662,838	<b>6</b>
Germany	138 078,334	1 848,881	<b>1</b>
France	106 199,337	626,000	<b>1</b>
Austria	9 914,359	570,544	<b>6</b>
Czech Republic	13 034,071	361,813	<b>3</b>

# Organic waste



Separation/Treatment



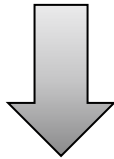
Fine fraction  
0-35 mm



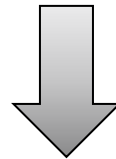
Coarse fraction  
> 35 mm

# Overview digester types

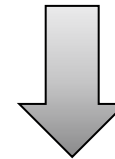
Green waste and organic residues



Wet fermentation



Plug flow fermenter



Box fermentation



# Wet fermentation



- Wet fermentation < 10 % TS
  - Digester with settling sediment collector
  
- Upstream system
  
- CSTR incl. „window“



# Plug flow digesters



- Dry digestion > 15 % TS





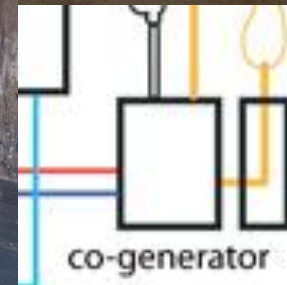
# Box digesters



- Percolation
- 30 – 50 % digestate and percolate



concrete di  
with integrated h



# Biogas Vienna



**capacity:** 17.000 t/a (upgradeable up to 34.000 t/a)

**technology:**

Processing, mashing, two-stage floating technique, dewatering, biogas utilization for district heating, exhaust air treatment, fermented residual preparation for composting

**gas production:**

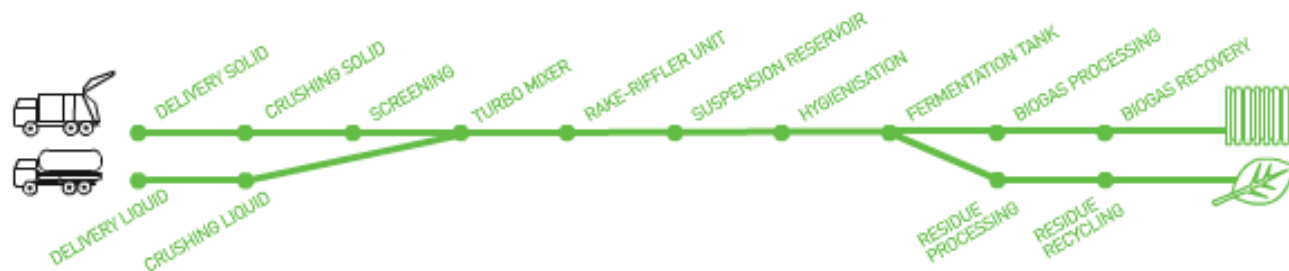
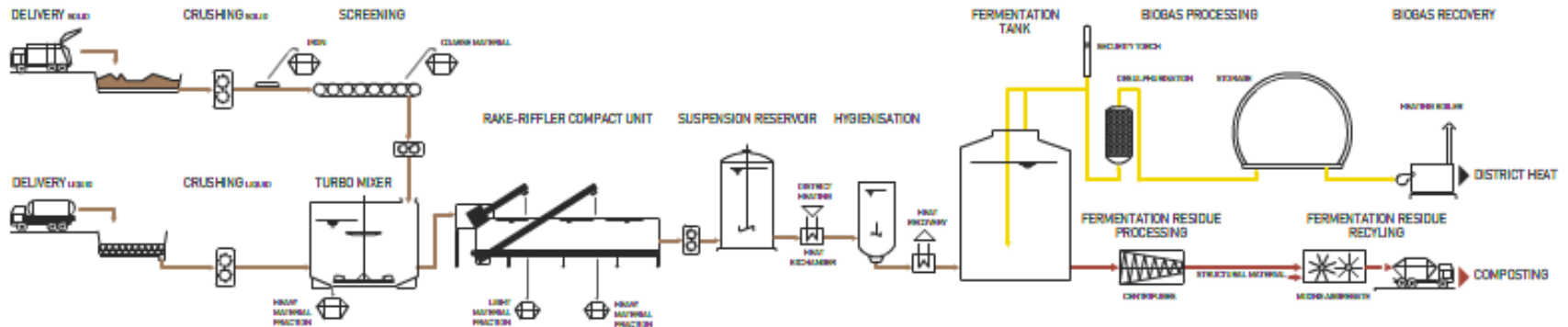
1.125.000 Nm<sup>3</sup>/a CH<sub>4</sub>  
(first expansion stage)

**energy transform method:**

Hot water boiler technology for district heating (for 300 households)

**costs:** 13,5 Mio. €

# Process scheme biogas Vienna



# Suspension Reservoir



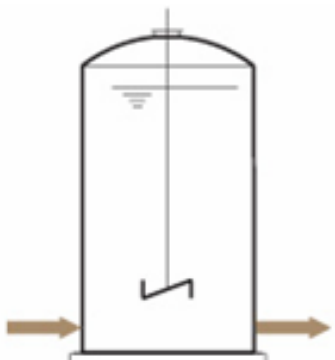
## SUSPENSION RESERVOIR

### TECHNICAL DATA:

Usable Volume

200 m<sup>3</sup>

The suspension reservoir provides constant feeding into the hygienisation facility. The contents of the container are mixed with a central stirring device in order to prevent sedimentation process.



Source: Rogalski, MA48, 2012

# Fermentation Tank

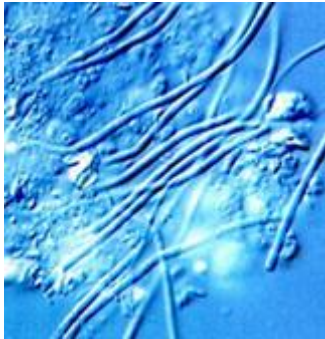
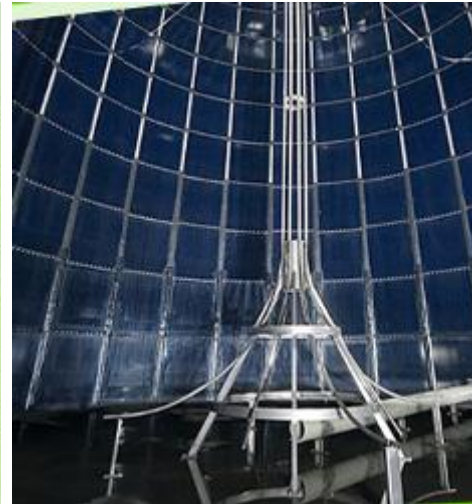


## FERMENTATION TANK

### TECHNICAL DATA:

Usable Volume	2.600 m <sup>3</sup>
Height	19 m
Diameter	14 m
Process	mesophile (37 - 40 °C)
Retention Time	20 days

Under anaerobic conditions, micro-organisms convert the organic ingredients from the waste suspension at the temperature from 37 to 40 °C into biogas.



Source: Rogalski, MA48, 2012



# Digestate management

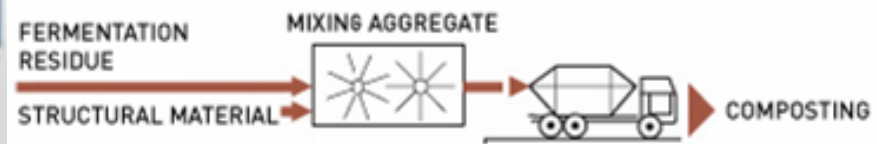


## TECHNICAL DATA: FERMENTATION RESIDUE RECYCLING

TECHNICAL DATA:	
<b>Bunker:</b>	
Usable Volume	60 m <sup>3</sup>
<b>Mixing Aggregate:</b>	
Power	55 kW
Mixing Ratio	1:1



The fermentation residue is mixed with structural material in a mixer, filled into containers and transported to the composting facility.



Source: Rogalski, MA48, 2012

# Lower Austria



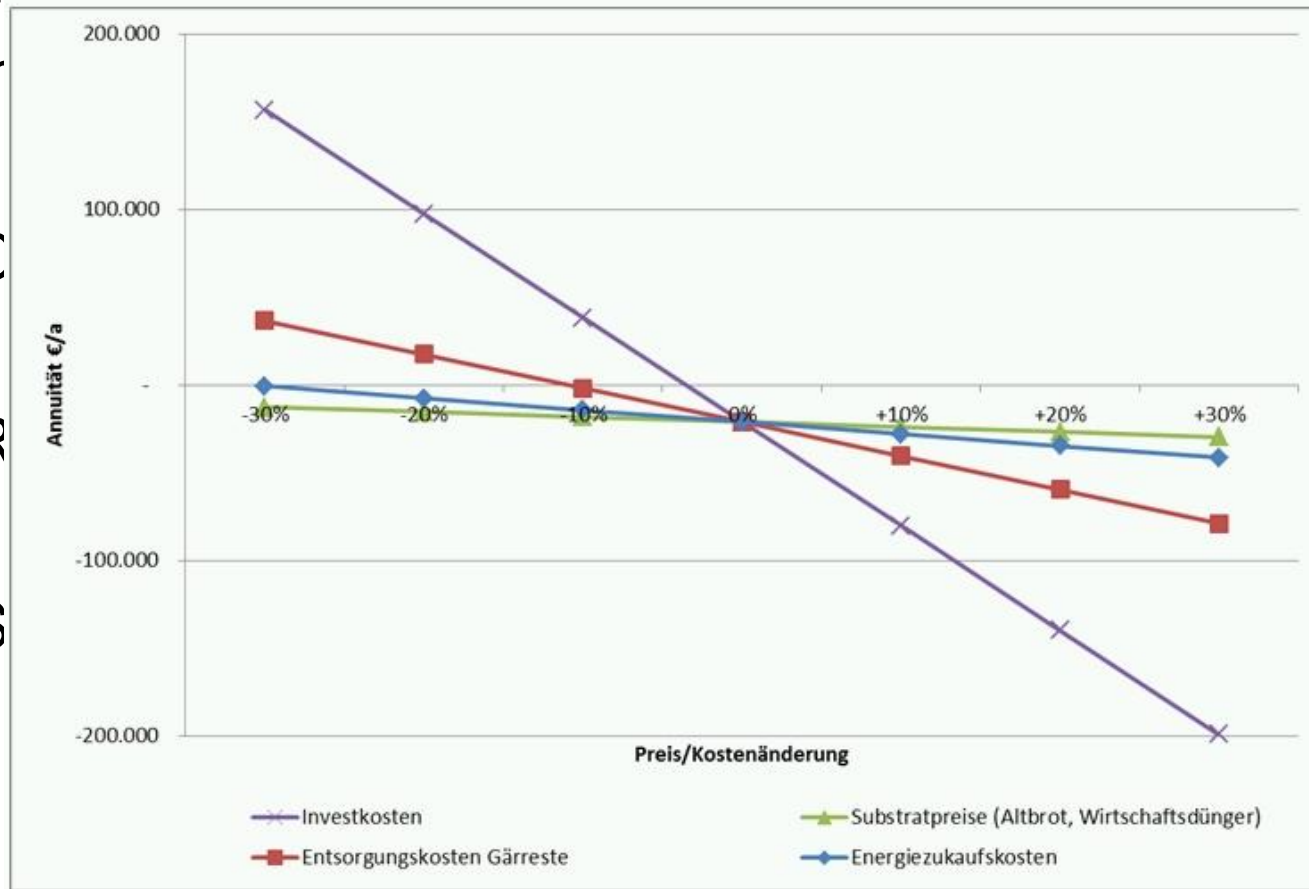
- Study about potentials
- 227,300 t/a biowaste
  - 17,000,000 Nm<sup>3</sup> CH<sub>4</sub> or 170 GWh
- 25 % of total biowaste potential
  - CHP 16,000 MWh<sub>el</sub> or 17,000 MWh<sub>therm</sub>
  - 0.15 % of electricity demand



# Costs

- 20 000 t/a → 10 000 t/a for biomass production

- Ir
- C
- R
- S



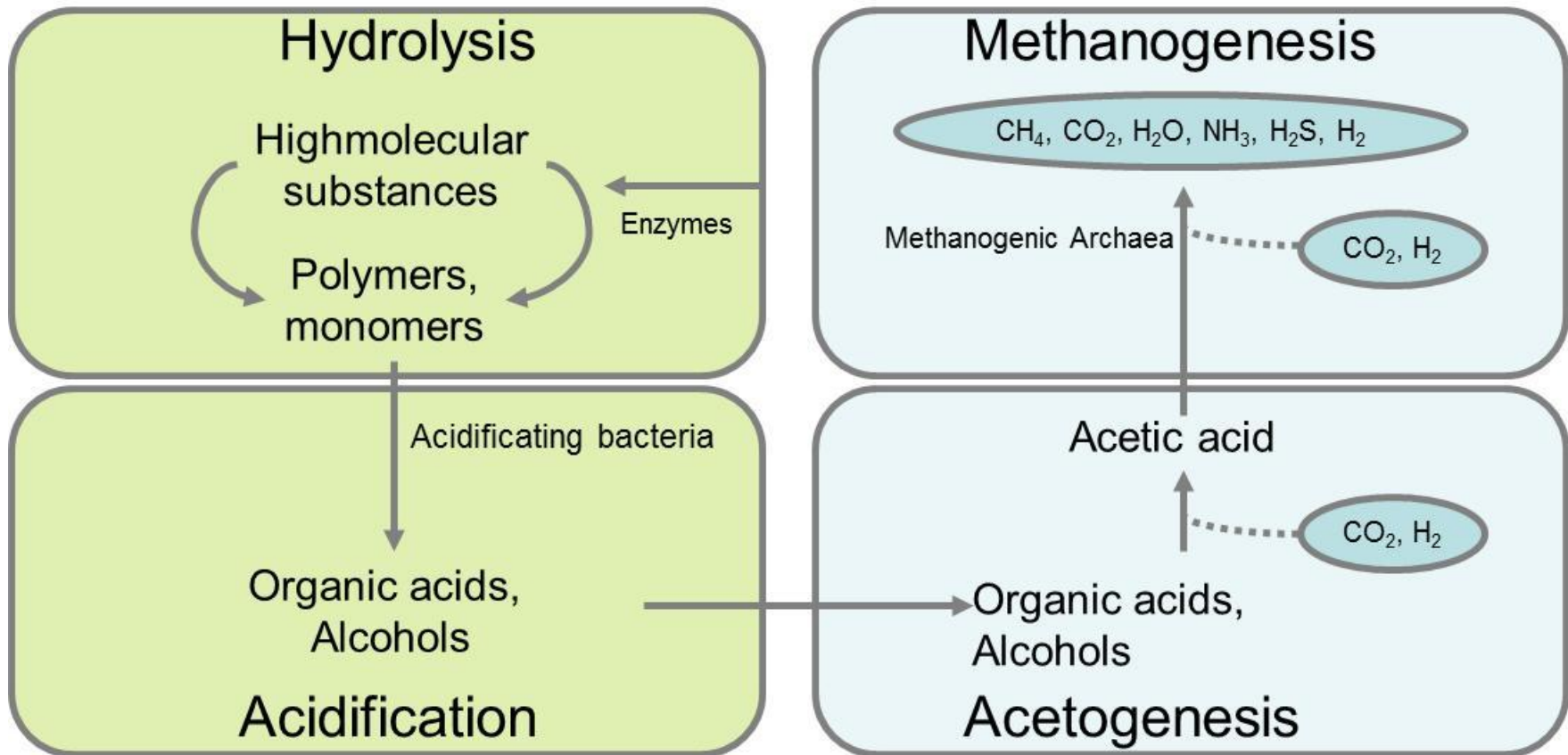


# ABE Fermentation



- Weizmann-process
- Heterofermentative organisms
- Fermentation of sugars
- Utilisation of acetic acid and butyric acid
- pH initiates the solventogenesis
- Production of acetone, butanol and ethanol
- Relation 3:6:1
- 12 – 20 g/L butanol
- Market price (650-1534€/t)

# 4 steps of AD

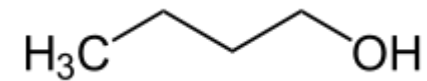




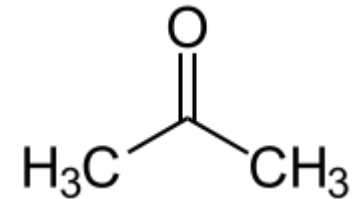
# Advantage of the products



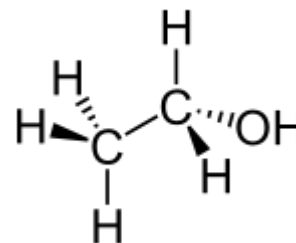
- Butanol
  - Widely used bulk chemical
  - Varnish, pharmaceutical industry, biofuel



- Acetone
  - Solvent
  - Inks, oils, plastics, varnish, resin, pharmaceutical industry



- Ethanol
  - Main alcohol
  - Solvent, biofuel, polypropylen



# Advantages ABE + biogas



- Combination with anaerobic digestion process
  - Digestion of residues
    - Biomass, unused compounds
    - Fermentation gases
  - Production of energy/process energy
  - Fertiliser
- Will it make the process economical feasible?

# Question?



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